

This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

1. (Currently Amended) A process for the treatment of a hydrocarbon charge containing resin, at least 80% of the compounds of ~~which have~~ the charge having a boiling point which is above or equal to 340°C, ~~in which said process comprising:~~
 - a) fractionating the charge ~~is sent to a fractionation stage during which the recovery takes place of to recover:~~
 - at least one heavy fraction comprising at least 90% by weight of compounds which boil at above 450°C and at below 700°C,
 - and at least one light fraction which boils at less than the heavy fraction(s),
 - a residuum which boils at more than the heavy fraction(s),
 - b) extracting at least part of the heavy fraction with a ~~paraffinic~~ paraffinic solvent having 3 to 7 carbon atoms, ~~is sent to an extraction stage during which to remove~~ at least some of the resins contained in said heavy fraction ~~are extracted and to recover~~ a purified resin depleted ~~fraction is recovered,~~
 - c) ~~a mixture is made which comprises at least part of the purified fraction obtained in the extraction stage~~ in a stage separate from the extracting stage (5) and after removal of said paraffinic solvents from said resin-depleted heavy fraction, mixing directly at least part of the resin-depleted heavy fraction with at least one light fraction obtained in the fractionation stage, and
 - d) passing the resultant mixture ~~thus obtained is sent~~ to a cracking stage.
2. (Original) A process according to Claim 1, in which the content of resins in the 340°C-700°C fraction of the charge is between 3 and 15% by weight.

3. (Previously Presented) A process according to claim 1, in which the heavy fraction resulting from the first fractionation stage comprises a resin content of more than 5% by weight.
4. (Previously Presented) A process according to claim 1, in which at least 20% by weight of the resins contained in the heavy fraction is extracted.
5. (Previously Presented) A process according to claim 1, in which the extraction of the resins of the heavy fraction makes it possible to obtain a purified fraction with a content of polyaromatic compounds comprising up to 5 cycles of less than 2% by weight.
6. (Previously Presented) A process according to claim 1, in which the extraction of the resins of the heavy fraction makes it possible to obtain a purified fraction, the nitrogen content of which is reduced by at least 20% by weight in relation to the heavy fraction which was introduced in the extraction stage.
7. (Previously Presented) A process according to claim 1, in which the extraction stage is carried out in an extraction column, using propane, under the following operating conditions :
 - a solvent ratio of between 2/1 and 12/1,
 - a temperature at the head of the extractor of between 55 and 95°C,
 - a temperature at the bottom of the extractor of between 30 and 80°C,
 - a pressure in the extractor of between 300 and 400 MPa, and
 - between 2 and 5 theoretical stages.
8. (Previously Presented) A process according to claim 1, in which the cracking stage is hydrocracking.

9. (Original) A process according to Claim 8, in which a residuum fraction is obtained from the hydrocracking stage and is sent, at least in part, to a dewaxing and hydrofinishing section for making oil bases.
10. (Previously Presented) A process according to claim 1, in which a residuum fraction is obtained from the hydrocracking stage and is sent, at least in part, to an FCC unit.
11. (Previously Presented) A process according to claim 8, in which a residuum fraction is obtained from the hydrocracking stage, and is recycled, at least in part, to the hydrocracking stage.
12. (Previously Presented) A process according to claim 1, in which the cracking stage is catalytic cracking in fluidised bed (FCC).
13. (Original) A process according to Claim 12, in which the FCC stage is preceded by a hydrotreatment stage.
14. (Previously Presented) A process according to claim 1, in which the charge is selected from a direct distillation residuum, a residuum from a conversion process, a coking residuum, a residuum from a hydroconversion process in fixed bed, a residuum from a conversion process in boiling bed, or a mixture of any one of these.
15. (Previously Presented) A process according to claim 1, in which an external charge is added to the heavy fraction entering the extraction stage, said charge being a vacuum distillate or an aromatic extract.
16. (Previously Presented) A process according to claim 1, wherein the parafinic solvent has 3 to 5 carbon atoms.

17. (Previously Presented) A process according to claim 1, wherein the paraffinic solvent is a heptane.
18. (New) A process for the treatment of a hydrocarbon charge containing resin, at least 80% of the compounds of the charge having a boiling point which is above or equal to 340°C, said process comprising:
- a) fractionating the charge to recover
 - at least one heavy fraction comprising at least 90% by weight of compounds which boil at above 450°C and at below 700°C,
 - and at least one light fraction which boils at less than the heavy fraction(s),
 - a residuum which boils at more than the heavy fraction(s),
 - b) extracting at least part of the heavy fraction with a paraffinic solvent having 3 to 7 carbon atoms, to remove at least some of the resins contained in said heavy fraction and to recover a resin-depleted fraction,
 - c) mixing directly at least part of the resin-depleted heavy fraction with at least part of the purified fraction obtained in the extraction stage and at least one light fraction obtained in the fractionation stage, and
 - d) passing the resultant mixture to a cracking stage.